

# SOLVENT REDUCED PROCESS FOR FLUORINE-FREE THICK ELECTRODES IN STATIONARY SODIUM-ION BATTERIES

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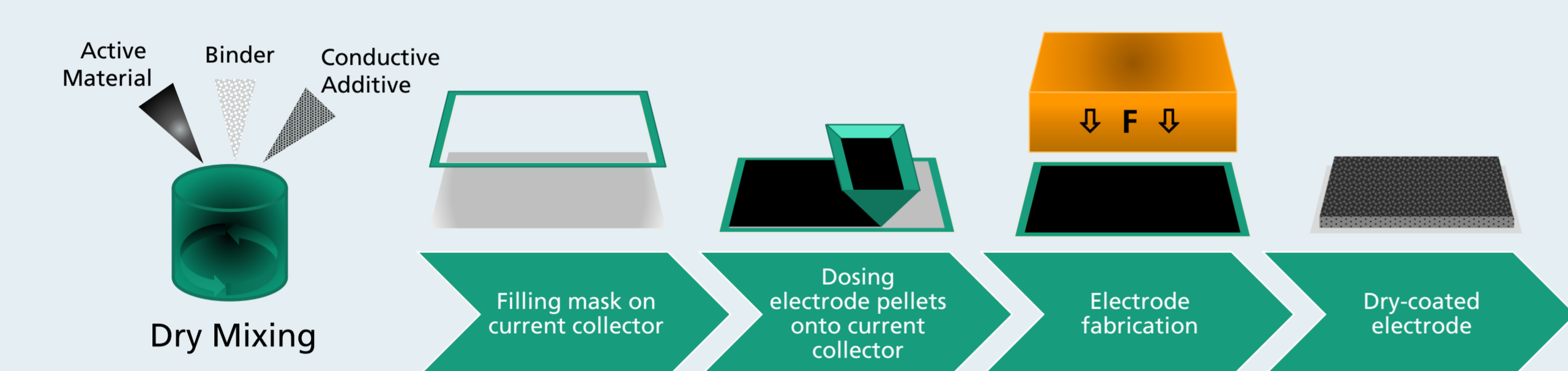
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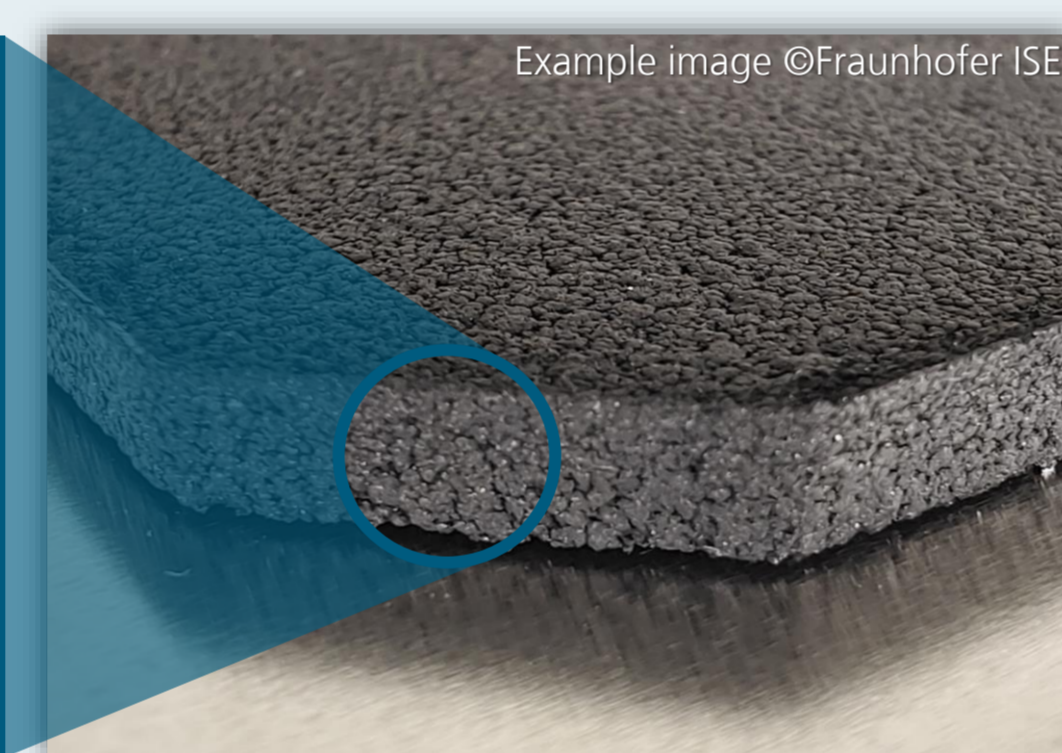
## Motivation

Sodium-ion batteries (SIBs) have recently attracted rising attention due to the use of highly available and globally evenly distributed **raw materials**, potential low **cost**, and convincing **performance**. Dry electrode processing for SIBs can enable higher specific energies and reduce costs, whilst showing potential to use fluorine-free binders without the need for *N*-methyl-2-pyrrolidone (NMP). Herein, we show promising results for this approach, using a **fluorine-free binder** with **P2-Na<sub>2/3</sub>Fe<sub>1/2</sub>Mn<sub>1/2</sub>O<sub>2</sub>** (NFMO) as cathode active material and **bio-based Hard Carbons** (HC) in **SIB full-cells** with areal capacities **>4 mAh·cm<sup>-2</sup>**.

## Morphology Tuned Thick Electrode Dry Processing



- Ultra-thick electrodes (~0.2 – 5 mm)
- Tunable porous structure
- Tunable pore & solid fraction sizes
- Tailored diffusion for ultra-high loadings
- Increased specific energy



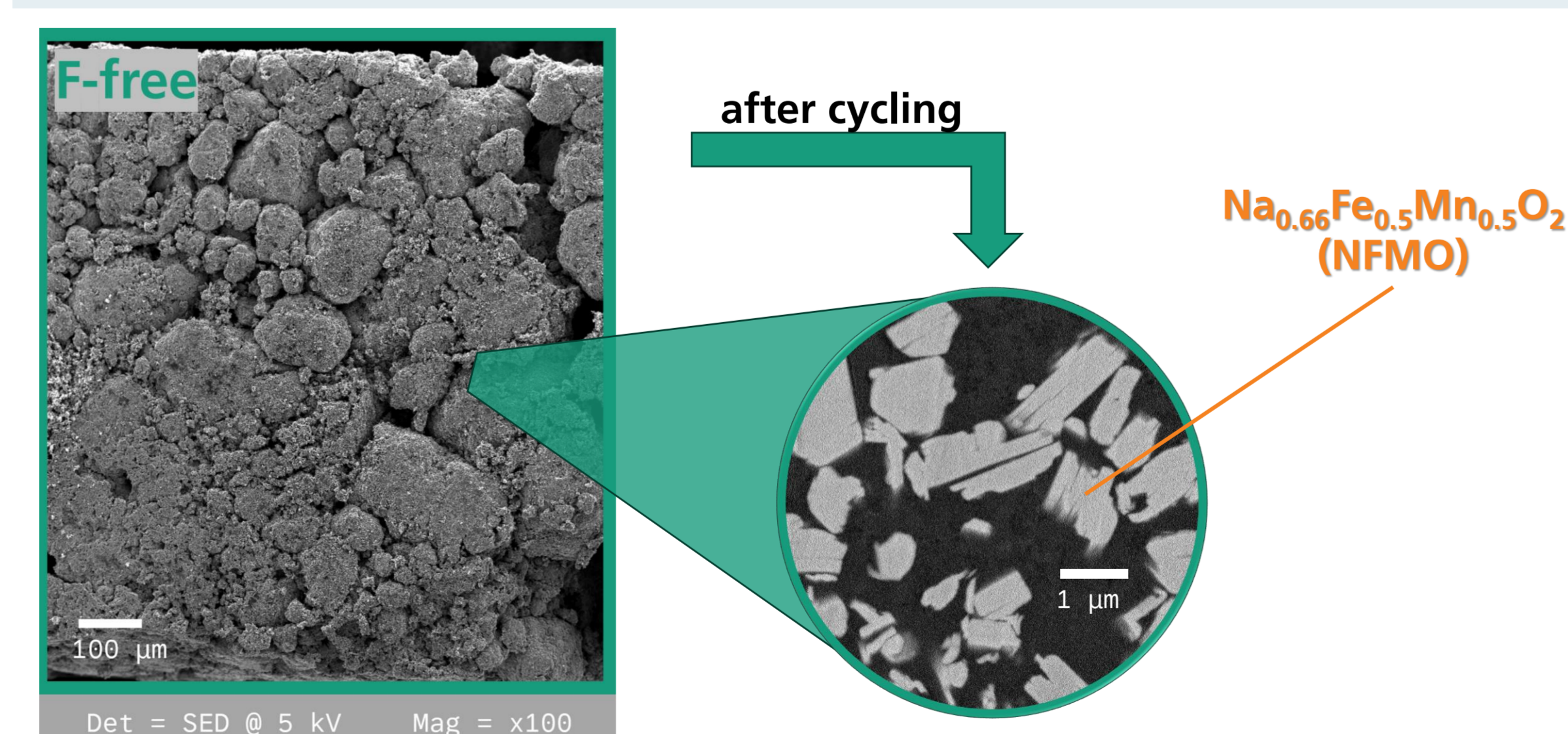
## Properties of Dry-Coating Process

### Pros

- + Possibility of thick electrodes with high areal capacity & specific energy
- + Solvent-free processing reduces production costs
- + No toxic solvents & no expensive NMP
- + Flexible material composition for flexible cell chemistries
- + Many possible binders

### Challenges

- Electronic/ionic conductivity & C-rate capability
- Higher binder & conductive additive content



## Experimental – Electrode Preparation

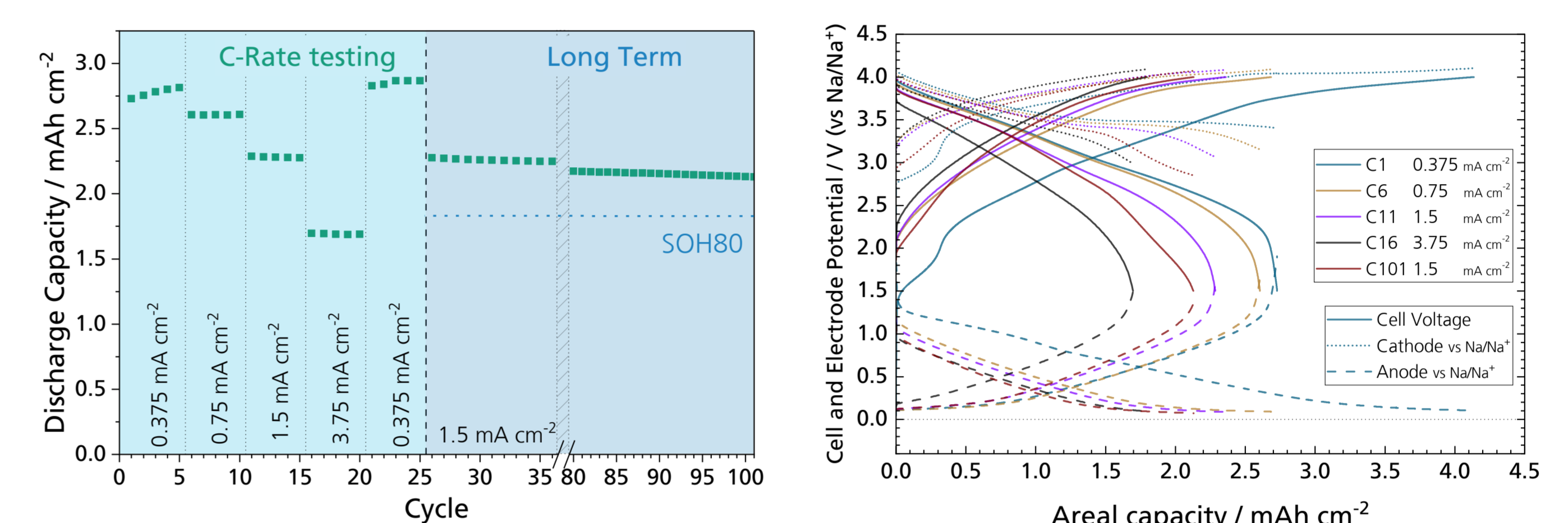
- 80% P2-Na<sub>2/3</sub>Fe<sub>1/2</sub>Mn<sub>1/2</sub>O<sub>2</sub> (MSE Supplies) & Cellulose-derived Hard Carbon (Fraunhofer ISE)
- Dry-mixed (12% Carbon Black, 8% fluorine-free binder) and structured
- Pressed on Al current collectors
- 18 mm electrodes (<1 mm thickness)

## Experimental – Electrochemical Characterization

- Hot-pressed electrodes in EL-CELL® PAT-Cells with 30 μm Delfort IonPort® SC-3042 Cellulose separator, 1M NaPF<sub>6</sub> in EC:DMC (3:7) + 4 % Additives (450 μl) as electrolyte
- Galvanostatic cycling in full-cells (vs. HC) **1.5 – 4.0 V** or **1.5 – 4.25 V**

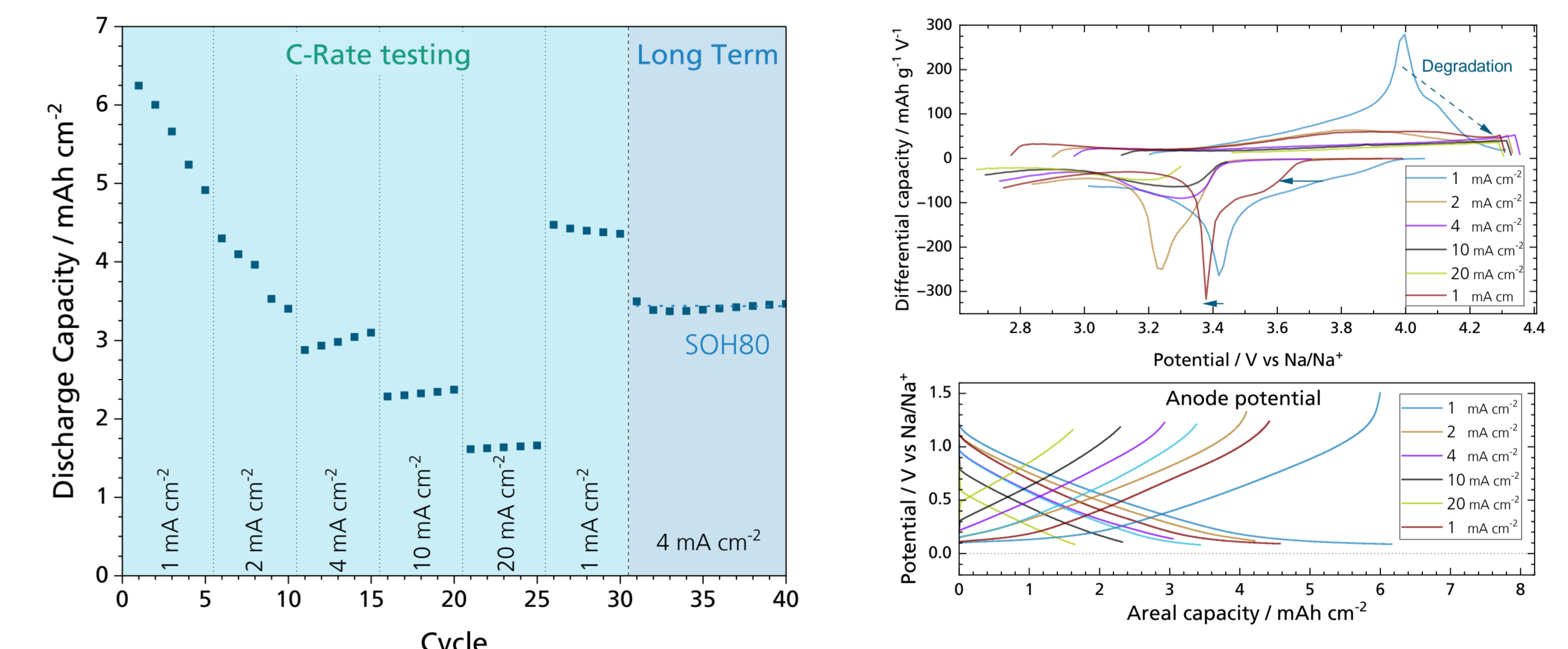
## Results – P2-Na<sub>2/3</sub>Fe<sub>1/2</sub>Mn<sub>1/2</sub>O<sub>2</sub> || Hard Carbon Full Cells

### Operating Window 1.5 – 4.0V: Non-plating behavior



- Relatively high initial losses:  $iCE = 66\%$  or  $70\text{ mAh g}_{HC}^{-1}$
- No Na-Metal plating at up to  $3.75\text{ mA cm}^{-2}$
- Stable capacities, limited C-Rate capability
- Relatively high overpotentials in cathode for higher currents

### Operating Window 1.5 – 4.25V: P2-NFMO Degradation and Anode Potential



- No Na-Metal plating at currents of up to  $20\text{ mA cm}^{-2}$
- NFMO: P2-OP4 phase transition  $>4\text{ V}$ 
  - Significant loss of capacity
  - Increased hysteresis and slower kinetics

## Conclusion & Outlook

- ✓ Successful application of fluorine-free binder for dry processed cathodes for SIBs enabling capacities  $>4\text{ mAh cm}^{-2}$
- ✓ Effective suppression of Na-Metal plating at high areal currents of  $20\text{ mA g}^{-1}$
- ⌚ Degradation of NFMO  $>4\text{ V}$  due to phase transition
- ⌚ Insufficient initial Coulombic Efficiencies
  - Optimization of electrode composition (binder & conductive additive)
  - Active material optimization
  - Electrolyte evaluation

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